



### 1.1 Use of ecofriendly HFO refrigerants

The most commonly used refrigerants in recent past were R11, R12, and R22 which because of their high ODP have been either phased out or under consideration for the same. After the revelation of the harmful effects of CFC and HCFC refrigerants on the ozone layer, search to find alternative working fluids gained more interest in the recent few years. The HFC134a was found to be a suitable candidate for replacing R12 and is being successfully used to date in small equipment like domestic refrigerators and water coolers and in mobile air-conditioning. HFC134a has very high GWP which is a matter of environmental concern [1]. HFO stands for hydro-fluoro-olefin (HFO-1234yf) is a low global warming potential (GWP) refrigerant for use in automotive air-conditioning systems. HFC-134a is a hydro-fluoro-carbon refrigerant, while (HFO-1234yf) is a hydro-fluoro-olefin refrigerant. Hydro-fluoro-olefin, or in short HFO, is a definition that is familiar to many of us. R1234yf, R1234ze are few examples of HFOs. They are used in a number of applications today, but have been barely studied just a decade ago. HFO-1234yf was developed to meet the European directive 2006/40/EC in 2011 requiring use of HFO refrigerant in AC system with a GWP below 150. HFO-1234yf, which has a 100-year GWP lower than 1. These refrigerants are used as a "near drop-in replacement" for R-134a, the current product used in automobile AC systems, which has a 100-year GWP of 1430. HFO-1234yf has the lowest cost among the currently proposed alternatives [2]. The initial cost of refrigeration and air conditioning system using R1234yf is much higher than that of R-134a and handled in repair shops in the same way as R-134a. Although it would require different, specialized equipment to perform the service due to the mild flammability of HFO-1234yf and another issue affecting the compatibility between HFO-1234yf and R-134a-based systems due to choice of lubricating oil. The current lubricating oil is showing signs of damage to plastic and aluminum, and issues with health, including mouth dryness, rashes, and sore throat, among other effects [3].

## 2. Literature Review

HFO-1234yf would be adopted as a replacement of R-134a automotive air-conditioning refrigerant. Mishra [2] concluded that the first law efficiency in terms of coefficient of performance COP and second law efficiency in terms of exergetic efficiency of HFC-134a and HFO-1234ze is almost same having a difference of 5.6%, which decreases with the increase in evaporator temperature, whereas it is 14.5-5% higher than HFO-1234yf. Hence HFO-1234yf can be a good drop-in' replacement of HFC-134a at higher value of evaporator temperature and HFO-1234ze can be a good replacement after certain modification. From the irreversibility or exergy destruction viewpoint, worst component is condenser followed by compressor, throttle valve, evaporator and liquid vapour heat exchanger, the most efficient component. Total efficiency defect is more for HFO-1234yf followed by HFO-1234ze and HFC-134a, but the difference is small. Increase in ambient state temperature has a increasing (positive) effect on second law efficiency in terms of exergetic

efficiency and exergy destruction ratio which was computed based on exergy of fuel or based on exergy of product (EDR). When exergy destruction ratio (EDR) reduced, then exergetic efficiency increases. Therefore HFO-1234yf gives lesser values of exergetic efficiency whereas HFO-1234ze gives approximately similar values. HFC-134a gives higher COP and exergetic efficiency than HFO-1234yf but lesser value than HFO-1234ze. However reverse trend is seen when effectiveness of heat exchanger is increased from 0 to 1. Hence, it can be concluded that even though the values of performance parameters for HFO-1234yf are smaller than that of HFC-134a, but the difference is small, so it can be a good alternative to HFC-134a because of its environmentally friendly properties. However HFO-1234ze can replace the conventional HFC-134a after having slight modification in the design as the performance parameters are almost similar [2].

### 2.1 Energy Exergy Analysis of Vapour Compression Refrigeration Systems

The second law analysis (i.e. exergy Computation) is widely accepted as a useful tool for obtaining overall performances of any system for finding various exergy losses occurred in its components. Exergy analysis also helps in taking account the important engineering decisions regarding design parameters of a system by finding maximum exergy destruction using entropy generation principle. Many researchers have carried out exergy studies of different thermal energy conversion systems describing various approach for exergy analysis and its usefulness for improving existing designs by reducing exergy destruction in a more simple and effective manner [1-3]. Padilla et al. [4] computed the exergy performance of a domestic vapor compression refrigeration system (VCRS) by using zeotropic mixture (R413A) for direct replacement of R12 and found that the overall energy and exergy performances of this system working with R413A is far better than R12. Arora and Kaushik [5] presented a detailed exergy analysis of an actual vapour compression refrigeration (VCR) cycle and developed computational model for computing coefficient of performance (COP), exergy destruction, exergetic efficiency and efficiency defects for R502, R404A and R507A and found that the R507A is a better substitute to R502 than R404A. The efficiency defect in condenser is highest, and lowest in liquid vapour heat exchanger for R502, R404A and R507A refrigerants in the range of  $-50^{\circ}\text{C}$  to  $0^{\circ}\text{C}$  evaporator temperature and in the range and  $40^{\circ}\text{C}$  to  $55^{\circ}\text{C}$  condenser temperature respectively. Anand S and Tyagi S. K. [6] presented a detailed experimental analysis of 2 ton of refrigeration capacity vapor compression refrigeration cycle using R22 as working fluid for different percentage of refrigerant charge using exergy analysis and evaluated thermal performances (i.e. coefficient of performance, exergy destruction, and exergetic efficiency) under variable quantity of refrigerant and found that the losses in the compressor are more pronounced, while the losses in the condenser are less pronounced as compared to other components. A computational model based on the exergy analysis is presented by Yumrutas et. al [7] for the investigation of the effects of the evaporating and condensing

temperatures on the pressure losses, exergy losses, second law of efficiency, and the COP of a vapour compression cycle. Dincer<sup>[8]</sup> asserts that conventional energy analysis, based on the first law of thermodynamics, evaluates energy mainly on its quantity but analysis that are based on second law considers not only the quality of energy, but also quantity of energy. Kumar et al. <sup>[9]</sup> also carried out to carry out the exergetic analysis of a VCR system using R11 and R12 as refrigerants. Nikolaidis and Probert [10] used exergy method for computing thermodynamic performances of R22 in a two-stage compound compression cycle, with flash intercooling.

Getu and Bansal [11] had optimized the design and operating parameters of like condensing temperature, subcooling temperature, evaporating temperature, superheating temperature and temperature difference in cascade heat exchanger R744-R717 cascade refrigeration system. A regression analysis was also done to obtain optimum thermodynamic parameters of same system.

From the irreversibility or exergy destruction viewpoint, worst component is condenser followed by compressor, throttle valve, evaporator and liquid vapour heat exchanger, the most efficient component. Total efficiency defect is more for HFO-1234yf followed by HFO-1234ze and HFC-134a, but the difference is small. Increase in ambient state temperature has a increasing (positive) effect on second law efficiency in terms of exergetic efficiency and exergy destruction ratio which was computed based on exergy of fuel or based on exergy of product (EDR). When exergy destruction ratio (EDR) reduced, then the exergetic efficiency increases. Therefore HFO-1234yf gives lesser values of exergetic efficiency whereas HFO-1234ze gives approximately 4% less values. HFC-134a gives higher COP and exergetic efficiency than HFO-1234yf but lesser value than HFO-1234ze [12].

Based on the literature it was observed that Researchers have gone through detailed first law analysis in terms of coefficient of performance and second law analysis in term of exergetic efficiency of simple vapour compression refrigeration system with single evaporator. Authors also analyzed the effect of nanofluids on simple vapour compression cycle in the term of pool boiling, COP, Thermal conductivity etc Researchers did not go through the irreversibility analysis or second law analysis of multiple evaporators systems with multi-stage expansion in vapour compression refrigeration systems.

### 3. Energy and exergy analysis

For carrying out energetic and exergetic analysis, computational models of system-1 to system-4 has been developed and impact of chosen refrigerants on these systems has been analyzed Exergy at any state is given as

$$X = (\Phi - \Phi_0) - T_0(s - s_0) \tag{1}$$

#### 3.1 Energy analysis

First law of thermodynamic gives the idea of energy balance of system.

##### Mass flow analysis of systems

$$\dot{m}_{c1} = \dot{m}_{e1} = \frac{\dot{Q}_{e1}}{(\Phi_1 - \Phi_{10})} \tag{2}$$

$$\dot{m}_{e2} = \frac{\dot{Q}_{e2}}{(\Phi_3 - \Phi_9)} \tag{3}$$

$$\dot{m}_{f1} = \frac{\dot{m}_{c1}(\Phi_2 - \Phi_3)}{(\Phi_3 - \Phi_9)} \tag{4}$$

$$\dot{m}_{c2} = \dot{m}_{c1} + \dot{m}_{e2} + \dot{m}_{f1} \tag{5}$$

$$\dot{m}_{e3} = \frac{\dot{Q}_{e3}}{(\Phi_5 - \Phi_8)} \tag{6}$$

$$\dot{m}_{f2} = \frac{\dot{m}_{c2}(\Phi_4 - \Phi_5)}{(\Phi_5 - \Phi_8)} \tag{7}$$

$$\dot{m}_{c3} = \dot{m}_{c2} + \dot{m}_{e3} + \dot{m}_{f2} \tag{8}$$

##### Energy consumption for systems

$$P_{c1} = \frac{\dot{m}_{c1}(\Phi_2 - \Phi_1)}{60} \tag{9}$$

$$P_{c2} = \frac{\dot{m}_{c2}(\Phi_4 - \Phi_3)}{60} \tag{10}$$

$$P_{c3} = \frac{\dot{m}_{c3}(\Phi_6 - \Phi_5)}{60} \tag{11}$$

##### Energetic efficiency of system-1

$$COP = \frac{\dot{Q}_e}{P_c * 60} \tag{12}$$

#### 3.2 Rate of exergy loss due to irreversibility ( $T_0\dot{S}_{gen}$ ) in various components of system-1

The concept of exergy was given by second law of thermodynamics, which always decreases due to thermodynamic irreversibility. Exergy is defined as the measure of usefulness, quality or potential of a stream to cause change and an effective measure of the potential of a substance to impact the environment [12].

##### Compressors

$$(T_0\dot{S}_{gen})_{c1} = \dot{W}_{c1} + \dot{m}_{c1}(X_2 - X_1) \tag{13}$$

$$(T_0\dot{S}_{gen})_{c2} = \dot{W}_{c2} + \dot{m}_{c2}(X_4 - X_3) \tag{14}$$

$$(T_0\dot{S}_{gen})_{c3} = \dot{W}_{c3} + \dot{m}_{c3}(X_6 - X_5) \tag{15}$$

$$\dot{\Psi}_c = (T_0\dot{S}_{gen})_{c1} + (T_0\dot{S}_{gen})_{c2} + (T_0\dot{S}_{gen})_{c3} \tag{16}$$

Evaporators

$$(T_o \dot{S}_{gen})_{e1} = \dot{m}_{e1}(X_1 - X_{10}) - \dot{Q}_{e1} \left(1 - \frac{T_0}{T_{r1}}\right) \quad (17)$$

$$(T_o \dot{S}_{gen})_{e2} = \dot{m}_{e2}(X_3 - X_9) - \dot{Q}_{e2} \left(1 - \frac{T_0}{T_{r2}}\right) \quad (18)$$

$$(T_o \dot{S}_{gen})_{e3} = \dot{m}_{e3}(X_5 - X_8) - \dot{Q}_{e3} \left(1 - \frac{T_0}{T_{r3}}\right) \quad (19)$$

$$\dot{\Psi}_e = (T_o \dot{S}_{gen})_{e1} + (T_o \dot{S}_{gen})_{e2} + (T_o \dot{S}_{gen})_{e3} \quad (20)$$

Condenser

$$\begin{aligned} \dot{\Psi}_{cond} &= (T_o \dot{S}_{gen})_{cond} \\ &= \dot{m}_{c3}(X_6 - X_7) - \dot{Q}_e \left(1 - \frac{T_0}{T_r}\right) \end{aligned} \quad (21)$$

Throttle Valves

$$(T_o \dot{S}_{gen})_{tv1} = \dot{m}_{e1}(X_{77} - X_{10}) \quad (22)$$

$$(T_o \dot{S}_{gen})_{tv2} = (\dot{m}_{e2} + \dot{m}_{f1})(X_{77} - X_9) \quad (23)$$

$$(T_o \dot{S}_{gen})_{tv3} = (\dot{m}_{e3} + \dot{m}_{f2})(X_{77} - X_8) \quad (24)$$

$$\begin{aligned} \dot{\Psi}_{tv} &= (T_o \dot{S}_{gen})_{tv1} + (T_o \dot{S}_{gen})_{tv2} \\ &\quad + (T_o \dot{S}_{gen})_{tv3} \end{aligned} \quad (25)$$

Liquid subcooler

$$\dot{\Psi}_{lsc} = (T_o \dot{S}_{gen})_{sc} = \dot{m}_{c3}(X_7 - X_{77}) \quad (26)$$

Flash intercoolers

$$(T_o \dot{S}_{gen})_{f1} = \dot{m}_{f1}(X_9 - X_3) + \dot{m}_{c1}(X_2 - X_3) \quad (27)$$

$$(T_o \dot{S}_{gen})_{f2} = \dot{m}_{f2}(X_8 - X_5) + \dot{m}_{c1}(X_4 - X_5) \quad (28)$$

$$\dot{\Psi}_f = (T_o \dot{S}_{gen})_{f1} + (T_o \dot{S}_{gen})_{f2} \quad (29)$$

Total irreversibility destruction in system-1

$$\sum \dot{\Psi}_k = \dot{\Psi}_e + \dot{\Psi}_c + \dot{\Psi}_{cond} + \dot{\Psi}_{tv} + \dot{\Psi}_{lsc} + \dot{\Psi}_f \quad (30)$$

$$\dot{m}_{c1} = \dot{m}_{e1} = \frac{\dot{Q}_{e1}}{(\Phi_1 - \Phi_{12})} \quad (31)$$

$$\dot{m}_{e2} = \frac{\dot{Q}_{e2}}{(\Phi_3 - \Phi_{10})} + \dot{m}_{c1} \left(\frac{x_{10'}}{1 - x_{10'}}\right) \quad (32)$$

$$\dot{m}_{f1} = \frac{\dot{m}_{c1}(\Phi_2 - \Phi_3)}{(\Phi_3 - \Phi_{10})} \quad (33)$$

$$\dot{m}_{c2} = \dot{m}_{c1} + \dot{m}_{e2} + \dot{m}_{f1} \quad (34)$$

$$\dot{m}_{e3} = \frac{\dot{Q}_{e3}}{(\Phi_5 - \Phi_8)} + \dot{m}_{c2} \left(\frac{x_{8'}}{1 - x_{8'}}\right) \quad (35)$$

$$\dot{m}_{f2} = \frac{\dot{m}_{c2}(\Phi_4 - \Phi_5)}{(\Phi_5 - \Phi_8)} \quad (36)$$

Power required for running the compressors

$$P_{c1} = \frac{\dot{m}_{c1}(\Phi_2 - \Phi_1)}{60} \quad (37)$$

$$P_{c2} = \frac{\dot{m}_{c2}(\Phi_4 - \Phi_3)}{60} \quad (38)$$

$$P_{c3} = \frac{\dot{m}_{c3}(\Phi_6 - \Phi_5)}{60} \quad (39)$$

$$\text{Energetic efficiency} = \frac{\dot{Q}_{e'}}{P_c * 60} \quad (40)$$

3.3 Rate of exergy loss due to irreversibilities ( $T_o \dot{S}_{gen}$ ) in various components of system-2

Compressors

$$(T_o \dot{S}_{gen})_{c1'} = \dot{W}_{c1'} + \dot{m}_{c1'}(X_2' - X_1') \quad (41)$$

$$(T_o \dot{S}_{gen})_{c2'} = \dot{W}_{c2'} + \dot{m}_{c2'}(X_4' - X_3') \quad (42)$$

$$(T_o \dot{S}_{gen})_{c3'} = \dot{W}_{c3'} + \dot{m}_{c3'}(X_6' - X_5') \quad (43)$$

$$\begin{aligned} \dot{\Psi}_{c'} &= (T_o \dot{S}_{gen})_{c1'} + (T_o \dot{S}_{gen})_{c2'} \\ &\quad + (T_o \dot{S}_{gen})_{c3'} \end{aligned} \quad (44)$$

Evaporators

$$(T_o \dot{S}_{gen})_{e1'} = \dot{m}_{e1'}(X_1' - X_{12}') - \dot{Q}_{e1'} \left(1 - \frac{T_0}{T_{r1'}}\right) \quad (45)$$

$$(T_o \dot{S}_{gen})_{e2'} = \dot{m}_{e2'}(X_3' - X_{10}') - \dot{Q}_{e2'} \left(1 - \frac{T_0}{T_{r2'}}\right) \quad (46)$$

$$(T_o \dot{S}_{gen})_{e3'} = \dot{m}_{e3'}(X_5' - X_8') - \dot{Q}_{e3'} \left(1 - \frac{T_0}{T_{r3'}}\right) \quad (47)$$

$$\dot{\Psi}_{e'} = (T_o \dot{S}_{gen})_{e1'} + (T_o \dot{S}_{gen})_{e2'} + (T_o \dot{S}_{gen})_{e3'} \quad (48)$$

Condenser

$$\begin{aligned} \dot{\Psi}_{cond} &= (T_o \dot{S}_{gen})_{cond} \\ &= \dot{m}_{c3'}(X_6' - X_7') - \dot{Q}_{e'} \left(1 - \frac{T_0}{T_{r'}}\right) \end{aligned} \quad (49)$$

Throttle Valves

$$(T_o \dot{S}_{gen})_{tv1} = \dot{m}_{e1'}(X_{11'} - X_{12'}) \quad (50)$$

$$(T_o \dot{S}_{gen})_{tv2} = \dot{m}_{c2'}(X_{9'} - X_{10'}) \quad (51)$$

$$(T_o \dot{S}_{gen})_{tv3} = \dot{m}_{c3'}(X_{77'} - X_{8'}) \quad (52)$$

$$\dot{\Psi}_{tv} = (T_o \dot{S}_{gen})_{tv1} + (T_o \dot{S}_{gen})_{tv2} + (T_o \dot{S}_{gen})_{tv3} \quad (53)$$

Liquid subcooler

$$\dot{\Psi}_{lsc} = (T_o \dot{S}_{gen})_{lsc} = \dot{m}_{c3'}(X_{7'} - X_{77'}) \quad (54)$$

Flash intercoolers

$$(T_o \dot{S}_{gen})_{f1'} = \dot{m}_{f1'}(X_{10'} - X_{3'}) + \dot{m}_{c1'}(X_{2'} - X_{3'}) \quad (55)$$

$$(T_o \dot{S}_{gen})_{f2'} = \dot{m}_{f2'}(X_{8'} - X_{5'}) + \dot{m}_{c2'}(X_{4'} - X_{5'}) \quad (56)$$

$$\dot{\Psi}_{f'} = (T_o \dot{S}_{gen})_{f1'} + (T_o \dot{S}_{gen})_{f2'} \quad (57)$$

Total irreversibility destruction in system-1

$$\sum \dot{\Psi}_{k'} = \dot{\Psi}_{e'} + \dot{\Psi}_{c'} + \dot{\Psi}_{cond'} + \dot{\Psi}_{tv'} + \dot{\Psi}_{lsc'} + \dot{\Psi}_{f'} \quad (58)$$

Exergetic efficiency

$$= \frac{\text{Exergy of cooling load of evaporators}}{\text{Compressors work}} = \frac{EP}{\dot{W}} \quad (59)$$

Exergetic efficiency of system

$$= \frac{(\dot{Q}_{e1} + \dot{Q}_{e2} + \dot{Q}_{e3}) - T_o \left( \frac{\dot{Q}_{e1}}{T_{r1}} + \frac{\dot{Q}_{e2}}{T_{r2}} + \frac{\dot{Q}_{e3}}{T_{r3}} \right)}{P_c * 60} \quad (60)$$

Rational efficiency of system - 2

$$= \frac{(\dot{Q}_{e1'} + \dot{Q}_{e2'} + \dot{Q}_{e3'}) - T_o \left( \frac{\dot{Q}_{e1'}}{T_{r1'}} + \frac{\dot{Q}_{e2'}}{T_{r2'}} + \frac{\dot{Q}_{e3'}}{T_{r3'}} \right)}{P_{c'} * 60} \quad (61)$$

3.4 Rate of exergy loss due to irreversibility ( $T_o \dot{S}_{gen}$ ) in various components of system-3

Compressors

$$(T_o \dot{S}_{gen})_{c1} = \dot{W}_{c1} + \dot{m}_{c1}(X_2 - X_1) \quad (63)$$

$$(T_o \dot{S}_{gen})_{c2} = \dot{W}_{c2} + \dot{m}_{c2}(X_4 - X_3) \quad (64)$$

$$(T_o \dot{S}_{gen})_{c3} = \dot{W}_{c3} + \dot{m}_{c3}(X_6 - X_5) \quad (65)$$

$$\dot{\Psi}_c = (T_o \dot{S}_{gen})_{c1} + (T_o \dot{S}_{gen})_{c2} + (T_o \dot{S}_{gen})_{c3} \quad (66)$$

Evaporators

$$(T_o \dot{S}_{gen})_{e1} = \dot{m}_{e1}(X_1 - X_{10}) - \dot{Q}_{e1} \left( 1 - \frac{T_o}{T_{r1}} \right) \quad (67)$$

$$(T_o \dot{S}_{gen})_{e2} = \dot{m}_{e2}(X_3 - X_9) - \dot{Q}_{e2} \left( 1 - \frac{T_o}{T_{r2}} \right) \quad (68)$$

$$(T_o \dot{S}_{gen})_{e3} = \dot{m}_{e3}(X_5 - X_8) - \dot{Q}_{e3} \left( 1 - \frac{T_o}{T_{r3}} \right) \quad (69)$$

$$\dot{\Psi}_e = (T_o \dot{S}_{gen})_{e1} + (T_o \dot{S}_{gen})_{e2} + (T_o \dot{S}_{gen})_{e3} \quad (70)$$

Condenser

$$\begin{aligned} \dot{\Psi}_{cond} &= (T_o \dot{S}_{gen})_{cond} \\ &= \dot{m}_{c3}(X_6 - X_7) - \dot{Q}_e \left( 1 - \frac{T_o}{T_r} \right) \end{aligned} \quad (71)$$

Throttle Valves

$$(T_o \dot{S}_{gen})_{tv1} = \dot{m}_{e1}(X_{77} - X_{10}) \quad (72)$$

$$(T_o \dot{S}_{gen})_{tv2} = (\dot{m}_{e2} + \dot{m}_{f1})(X_{77} - X_9) \quad (73)$$

$$(T_o \dot{S}_{gen})_{tv3} = (\dot{m}_{e3} + \dot{m}_{f2})(X_{77} - X_8) \quad (74)$$

$$\dot{\Psi}_{tv} = (T_o \dot{S}_{gen})_{tv1} + (T_o \dot{S}_{gen})_{tv2} + (T_o \dot{S}_{gen})_{tv3} \quad (75)$$

Liquid subcooler

$$\dot{\Psi}_{lsc} = (T_o \dot{S}_{gen})_{sc} = \dot{m}_{c3}(X_7 - X_{77}) \quad (76)$$

$$\dot{\Psi}_f = (T_o \dot{S}_{gen})_{f1} + (T_o \dot{S}_{gen})_{f2} \quad (77)$$

Total irreversibility destruction in system-3

$$\sum \dot{\Psi}_k = \dot{\Psi}_e + \dot{\Psi}_c + \dot{\Psi}_{cond} + \dot{\Psi}_{tv} + \dot{\Psi}_{lsc} + \dot{\Psi}_f \quad (78)$$

$$\dot{m}_{c1} = \dot{m}_{e1} = \frac{\dot{Q}_{e1}}{(\Phi_1 - \Phi_{12})} \quad (79)$$

$$\dot{m}_{e2} = \frac{\dot{Q}_{e2}}{(\Phi_3 - \Phi_{10})} + \dot{m}_{c1} \left( \frac{x_{10'}}{1 - x_{10'}} \right) \quad (80)$$

$$\dot{m}_{f1} = \frac{\dot{m}_{c1}(\Phi_2 - \Phi_3)}{(\Phi_3 - \Phi_{10})} \quad (81)$$

$$\dot{m}_{c2} = \dot{m}_{c1} + \dot{m}_{e2} + \dot{m}_{f1} \quad (82)$$

$$\dot{m}_{e3} = \frac{\dot{Q}_{e3}}{(\Phi_5 - \Phi_8)} + \dot{m}_{c2} \left( \frac{x_{8'}}{1 - x_{8'}} \right) \quad (83)$$

$$\dot{m}_{f2} = \frac{\dot{m}_{c2}(\Phi_4 - \Phi_5)}{(\Phi_5 - \Phi_8)} \quad (84)$$

Power required for running the compressors

$$P_{c1} = \frac{\dot{m}_{c1}(\Phi_2 - \Phi_1)}{60} \quad (85)$$

$$P_{c2} = \frac{\dot{m}_{c2}(\Phi_4 - \Phi_3)}{60} \quad (86)$$

$$P_{c3} = \frac{\dot{m}_{c3}(\Phi_6 - \Phi_5)}{60} \quad (87)$$

$$\text{Energetic efficiency} = \frac{\dot{Q}_{e'}}{P_c * 60} \quad (88)$$

### 3.5 Rate of exergy loss due to irreversibilities ( $T_0 \dot{S}_{gen}$ ) in various components of system-4

#### Compressors

$$(T_0 \dot{S}_{gen})_{c1'} = \dot{W}_{c1'} + \dot{m}_{c1'}(X_2' - X_1') \quad (89)$$

$$(T_0 \dot{S}_{gen})_{c2'} = \dot{W}_{c2'} + \dot{m}_{c2'}(X_4' - X_3') \quad (90)$$

$$(T_0 \dot{S}_{gen})_{c3'} = \dot{W}_{c3'} + \dot{m}_{c3'}(X_6' - X_5') \quad (91)$$

$$\dot{\Psi}_{c'} = (T_0 \dot{S}_{gen})_{c1'} + (T_0 \dot{S}_{gen})_{c2'} + (T_0 \dot{S}_{gen})_{c3'} \quad (92)$$

#### Evaporators

$$(T_0 \dot{S}_{gen})_{e1'} = \dot{m}_{e1'}(X_1' - X_{12}') - \dot{Q}_{e1'} \left(1 - \frac{T_0}{T_{r1'}}\right) \quad (93)$$

$$(T_0 \dot{S}_{gen})_{e2'} = \dot{m}_{e2'}(X_3' - X_{10}') - \dot{Q}_{e2'} \left(1 - \frac{T_0}{T_{r2'}}\right) \quad (94)$$

$$(T_0 \dot{S}_{gen})_{e3'} = \dot{m}_{e3'}(X_5' - X_8') - \dot{Q}_{e3'} \left(1 - \frac{T_0}{T_{r3'}}\right) \quad (95)$$

$$\dot{\Psi}_{e'} = (T_0 \dot{S}_{gen})_{e1'} + (T_0 \dot{S}_{gen})_{e2'} + (T_0 \dot{S}_{gen})_{e3'} \quad (96)$$

#### Condenser

$$\begin{aligned} \dot{\Psi}_{cond'} &= (T_0 \dot{S}_{gen})_{cond'} \\ &= \dot{m}_{c3'}(X_6' - X_7') - \dot{Q}_{e'} \left(1 - \frac{T_0}{T_{r'}}\right) \end{aligned} \quad (97)$$

#### Throttle Valves

$$(T_0 \dot{S}_{gen})_{tv1} = \dot{m}_{e1'}(X_{11}' - X_{12}') \quad (98)$$

$$(T_0 \dot{S}_{gen})_{tv2} = \dot{m}_{c2'}(X_9' - X_{10}') \quad (99)$$

$$(T_0 \dot{S}_{gen})_{tv3} = \dot{m}_{c3'}(X_{77}' - X_8') \quad (100)$$

$$\dot{\Psi}_{tv} = (T_0 \dot{S}_{gen})_{tv1} + (T_0 \dot{S}_{gen})_{tv2} + (T_0 \dot{S}_{gen})_{tv3} \quad (101)$$

#### Liquid subcooler

$$\dot{\Psi}_{lsc'} = (T_0 \dot{S}_{gen})_{lsc'} = \dot{m}_{c3'}(X_{77}' - X_{77}') \quad (102)$$

Total irreversibility destruction in system-1

$$\sum \dot{\Psi}_{k'} = \dot{\Psi}_{e'} + \dot{\Psi}_{c'} + \dot{\Psi}_{cond'} + \dot{\Psi}_{tv'} + \dot{\Psi}_{lsc'} + \dot{\Psi}_{f'} \quad (103)$$

Exergetic efficiency for system-4 can be expressed as

$$\begin{aligned} \text{Exergetic efficiency} \\ &= \frac{\text{Exergy of cooling load of evaporators}}{\text{Compressors work}} = \frac{\dot{E}P}{\dot{W}} \end{aligned} \quad (104)$$

Exergetic efficiency of system – 4 is

$$= \frac{(\dot{Q}_{e1} + \dot{Q}_{e2} + \dot{Q}_{e3}) - T_0 \left( \frac{\dot{Q}_{e1}}{T_{r1}} + \frac{\dot{Q}_{e2}}{T_{r2}} + \frac{\dot{Q}_{e3}}{T_{r3}} \right)}{P_c * 60} \quad (105)$$

## 4. Results and Discussion

Following systems have been considered for present investigations.

*System-1:* Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, individual expansion valves and flash inter coolers

*System-2:* Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves and flash inter coolers

*System-3:* Vapour compression refrigeration system using multiple evaporators at different temperatures with individual compressors, multiple expansion valves

*System-4:* Vapour compression refrigeration system using multiple evaporators at different temperatures with individual compressors, individual expansion valves.

Comparison were made of for above four systems with following input conditions using ecofriendly refrigerants for following input conditions

- Load on the low, intermediate and high temperature evaporators are 30TR, 20 TR and 10 TR respectively.
- Dead state temperature ( $T_0$ ): 25 °C
- Difference between evaporator and space temperature ( $T_r - T_e$ ): 5 °C.
- Adiabatic efficiency of compressor: 80%.
- Dead state enthalpy ( $\Phi_0$ ) and entropy ( $s_0$ ) of the refrigerants have been calculated corresponding to the dead state temperature ( $T_0$ ) of 25 °C.

- Variation in kinetic and potential energy is negligible.
- Expansion process is adiabatic
- Temperature of low, intermediate and high temperature evaporators are -5°C, 0 °C and 5°C respectively.
- Condenser temperature : 40 °C
- Degree of sub cooling : 10 °C

It is clear from Table-1, that vapour compression refrigeration system using R134a with multiple evaporators at different temperatures with individual compressors, multiple expansion valves (system-3) gives better thermodynamic performances with low electrical power required to run whole system) i.e. all compressors. It is also observed that exergy destruction in

condenser is highest. However the exergy destruction in all compressors is almost similar. Similarly exergy destruction in condensers in all almost similar. The exergy destruction in evaporators in System-2: Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves and flash inter coolers( system-2) is highest as compared to other systems. However exergy destruction in evaporators system-3 has less exergy destruction than system-2 but higher than system-1 and system-4. It is also observed that exergy destruction in flash chamber is lowest. exergy destruction in expansion valves of system-4 is higher than system-1, system-2 and system3.

Table 1(a): Thermodynamic performances of various vapour compression refrigeration systems using HFC-134a refrigerant

Performance parameters	System-1	System-2	System-3	System-4
First Law efficiency (COP_Actual)	4.297	4.428	4.593	4.291
Exergy Destruction Ratio (EDR)	1.961	2	1.894	1.965
Exergetic Efficiency using First Method	0.3377	0.3481	0.361	0.3373
Exergy of Fuel (kW)	48.87	47.42	45.72	48.94
Exergy of Product(kW)	16.51	16.51	16.51	16.51
Exergetic Efficiency using second Method	0.3329	0.3311	0.3108	0.3322
Sum of total Exergy Destruction in three Compressors (%)	23.82	23.82	23.15	23.13
Exergy Destruction in Condensers	24.28	24.5	24.89	24.23
Sum of total Exergy Destruction in three Evaporators (%)	7.411	14.45	14.07	7.218
Sum of total Exergy Destruction in three Expansion Valves (%)	8.91	4.857	4.322	9.823
Exergy Destruction in Subcooler (%)	1.749	1.945	1.931	1.871
Exergy Destruction in Flash chambers (%)	0.0513	0.042	Flash chambers not used	Not used Flash chambers
Second law efficiency	0.481	0.5073	0.5141	0.4803

#### 4.1 Effect of different Load conditions

Comparison were made of for above four systems with input conditions using ecofriendly refrigerants for following input conditions

1. Load on the low, intermediate and high temperature evaporators are 10TR, 20 TR and 30 TR respectively.
2. Dead state temperature ( $T_0$ ): 25 °C (i.e. 298K)
3. Difference between evaporator and space temperature ( $T_r - T_e$ ): 5 °C.

4. Adiabatic efficiency of compressor: 100%
5. Dead state enthalpy ( $\Phi_0$ ) and entropy ( $s_0$ ) of the refrigerants have been calculated corresponding to the dead state temperature ( $T_0$ ) of 25 °C (i.e. 298K)
6. Variation in kinetic and potential energy is negligible.
7. Expansion process is adiabatic
8. Temperature of low, intermediate and high temperature evaporators are -5 °C, 0 °C and 5 °C respectively.
9. Condenser temperature : 40 °C
10. Degree of sub cooling : 10 °C

Table 1(b): Thermodynamic performances of various vapour compression refrigeration systems using HFC-134a refrigerant

Performance parameters	System-1	System-2	System-3	System-4
First Law efficiency (COP_Actual)	4.807	4.87	4.983	4.79
Exergy Destruction Ratio (EDR)	2.164	2.201	2.134	2.175
Exergetic Efficiency using First Method	0.3161	0.3202	0.3276	0.3149
Exergy of Fuel (kW)	43.02	40.85	40.54	42.63
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergetic Efficiency using second Method	0.3161	0.2953	0.3007	0.3149
Total Exergy Destruction in Compressors (%)	23.53	23.57	23.21	23.2
Total Exergy Destruction in Condensers (%)	26.62	26.51	26.76	26.35
Exergy Destruction Evaporators (%)	9.683	13.6	13.55	9.65
Exergy Destruction in Expansion Valves(%)	6.615	4.653	4.31	7.25
Exergy Destruction in Subcooler(%)	1.902	2.105	2.1	2.063
Exergy Destruction in Flash chambers (%)	0.08	0.02	Not used Flash chambers	Not used Flash chambers

Comparison were made of for above four systems with input conditions using ecofriendly refrigerants for following input conditions

- Load on the low, intermediate and high temperature evaporators are 20TR, 30 TR and 10 TR respectively.
- Dead state temperature ( $T_0$ ): 25 °C

- Difference between evaporator and space temperature ( $T_r - T_e$ ): 5 °C.
- Adiabatic efficiency of compressor: 75%.
- Dead state enthalpy ( $\Phi_0$ ) and entropy ( $s_0$ ) of the refrigerants have been calculated corresponding to the dead state temperature ( $T_0$ ) of 25 °C.
- Variation in kinetic and potential energy is negligible.
- Expansion process is adiabatic
- Temperature of low, intermediate and high temperature evaporators are -5 °C, 0 °C and 5 °C respectively.
- Condenser temperature : 40 °C
- Degree of sub cooling : 10 °C

Table 1(c): Thermodynamic performances of various vapour compression refrigeration systems using HFC-134a refrigerant

Performance parameters	System-1	System-2	System-3	System-4
First Law efficiency (COP_Actual)	4.419	4.532	4.699	4.41
Exergy Destruction Ratio (EDR)	2.004	2.047	1.947	2.01
Exergetic Efficiency using First Method	0.3329	0.3414	0.354	0.3322
Exergy of Fuel (kW)	43.02	40.85	40.54	42.63
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergy Destruction in Compressors (%)	23.75	23.5	23.17	23.15
Exergy Destruction in Condensers (%)	24.84	24.73	25.32	24.75
Exergy Destruction Evaporators (%)	8.044	7.91	14.18	7.9
Exergy Destruction in Expansion Valves (%)	8.247	9.07	4.28	9.076
Exergy Destruction in Subcooler (%)	1.784	1.92	1.97	1.917
Exergy Destruction in Flash chambers (%)	0.05	0.051	Not used Flash chambers	Not used Flash chambers
Exergetic efficiency second methods efficiency	0.3329	0.3311	0.3108	0.3322

4.2 Effect of HFO-1234ze ecofriendly refrigerant

Case-1: In this investigation following assumptions are made by

using HFO-1234ze refrigerant shown in table-2. Similarly thermodynamic performances of various systems using R1234ze are shown in Table-2(b) to Table-2(d) respectively.

Table-2(a): Thermodynamic performances of various vapour compression refrigeration systems using HFO-1234ze refrigerant

Input Data	System-1	System-2	System-3	System-4
Refrigerant	HFO-1234ze	HFO-1234ze	HFO-1234ze	HFO-1234ze
Q_Eva1 (kW)	70	105	70	70
Q_Eva2 (kW)	105	70	105	105
Q_Eva3 (kW)	35	35	35	35
Temperature of Evaporator-1 (°C)	-5	-10	-10	-10
Temperature of Evaporator-2 (°C)	0	5	5	5
Temperature of Evaporator-3 (°C)	5	10	10	10
Temperature of condenser (°C)	40	40	40	40
Subcooling Temperature of condenser (°C)	30	30	30	30
Isentropic efficiency of compressors	0.75	0.75	0.75	0.75

vapour compression refrigeration system using multiple evaporators at different temperatures with individual compressors, multiple expansion valves (system-3) gives better thermodynamic performances with low electrical power required to run whole system) i.e. all compressors. It is also observed that exergy destruction in condenser is highest. However the exergy destruction in all compressors is almost similar. Similarly exergy destruction in condensers in all almost similar. The exergy destruction in evaporators in System-2: Vapour compression

refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves and flash inter coolers( system-2) is highest as compared to other systems. However exergy destruction in evaporators system-3 has less exergy destruction than system-2 but higher than system-1 and system-4. It is also observed that exergy destruction in flash chamber is lowest. exergy destruction in expansion valves of system-4 is higher than system-1, system-2 and system3.

Table 2(b): Thermodynamic performances of various vapour compression refrigeration systems using HFO-1234ze refrigerant

Performance parameters	System-1	System-2	System-3	System-4
First Law efficiency (COP_Actual)	4.881	5.141	5.18	4.926
Exergy Destruction Ratio (EDR)	2.415	2.338	2.313	2.383
Exergetic Efficiency using First Method	0.2929	0.3085	0.3108	0.2956
Exergy of Fuel (kW)	43.02	40.85	40.54	42.63
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergetic Efficiency using second Method	0.2929	0.2789	0.2956	0.2956
Second law efficiency (%)	64.96	68.42	0.6556	0.6556



Table 2(c): Exergy\_Destruction of various components in vapour compression refrigeration systems using HFO-1234ze refrigerant

Performance parameters	System-1	System-2	System-3	System-4
Total Exergy Destruction in compressors (%)	24.31	24.21	23.69	23.69
Total Exergy Destruction in condensers (%)	27.68	28.9	29.12	27.93
Total Exergy Destruction in evaporators (%)	7.756	11.12	11.2	7.827
Total Exergy Destruction in expansion Valves (%)	8.405	5.192	5.2	8.432
Total Exergy Destruction in sub coolers	2.565	2.698	2.68	2.568
Rational Efficiency (%)	29.29	27.89	29.56	29.56

Table (2d): Work done by each compressor in vapour compression refrigeration systems using HFO-1234ze refrigerant

Performance parameters	System-1	System-2	System-3	System-4
Work done by compressor -1 (kW)	2.498	1.862	8.025	10.77
Work done by compressor -2 (kW)	6.767	5.517	13.4	15.7
Work done by compressor 3 (kW)	33.76	33.47	19.1	16.16
Exergy of Fuel (kW)	43.02	40.85	40.54	42.63
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergetic Efficiency using second Method (%)	29.29	30.85	28.11	29.56

Case-2: In this investigation following assumptions are made by using HFO refrigerant shown in Table-3(a)

Table 3: Thermodynamic performances of various vapour compression refrigeration systems using HFO-1234yf refrigerant

Input Data	System-1	System-2	System-3	System-4
Refrigerant	R1234yf	R1234yf	R1234yf	R1234yf
Q_Eva1 (kW)	70	105	70	70
Q_Eva2 (kW)	105	70	105	105
Q_Eva3 (kW)	35	35	35	35
Temperature of Evaporator-1 (°C)	-5	-10	-10	-10
Temperature of Evaporator-2 (°C)	0	5	5	5
Temperature of Evaporator-3 (°C)	5	10	10	10
Temperature of condenser (°C)	40	40	40	40
Subcooling Temperature of condenser (°C)	30	30	30	30
Isentropic efficiency of compressors	0.75	0.75	0.75	0.75

vapour compression refrigeration system using multiple evaporators at different temperatures with individual compressors, multiple expansion valves (system-3) gives better thermodynamic performances with low electrical power required to run whole system) i.e. all compressors. It is also observed that exergy destruction in condenser is highest. However the exergy destruction in all compressors is almost similar. Similarly exergy destruction in condensers in all almost similar. The exergy destruction in evaporators in System-2: Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion

valves and flash inter coolers( system-2) is highest as compared to other systems. How ever exergy destruction in evaporators system-3 has less exergy destruction than system-2 but higher than system-1 and system-4. It is also observed that exergy destruction in flash chamber is lowest. exergy destruction in expansion valves of system-4 is higher than system-1, system-2 and system3.

Case-3: In this investigation following assumptions are made by using HFC-1234yf refrigerant:

Table 3(a): Thermodynamic performances of various vapour compression refrigeration systems using HFO-134a refrigerant

Input Data	System-1	System-2	System-3	System-4
Refrigerant	R134a	R134a	R134a	R134a
Q_Eva1 (kW)	70	105	70	70
Q_Eva2 (kW)	105	70	105	105
Q_Eva3 (kW)	35	35	35	35
Temperature of Evaporator-1 (°C)	-5	-10	-10	-10
Temperature of Evaporator-2 (°C)	0	5	5	5
Temperature of Evaporator-3 (°C)	5	10	10	10
Temperature of condenser (°C)	40	40	40	40
Subcooling Temperature of condenser (°C)	30	30	30	30
Isentropic efficiency of compressors	0.75	0.75	0.75	0.75

The exergy destruction in condenser is higher than compressor. For comparing all four systems, the exergy destruction in system-3 is high and lower in system-4 respectively. The exergy destruction in running all compressors of system-1 is highest while for system-4 is lowest. However the exergy destruction in all compressors is almost similar. Similarly exergy destruction in condenser in all systems is almost similar. The exergy destruction in evaporators in System-2: Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves and flash inter coolers (system-2) is highest as compared to other systems. However exergy destruction in evaporators system-3 has less exergy destruction than system-2 but higher than system-1 and

system-4. It is also observed that exergy destruction in flash chamber is lowest. exergy destruction in expansion valves of system-4 is higher than system-1, system-2 and system3.

Table-3(a) shows the exergy destruction in various components of vapour compression refrigeration systems using R-134a refrigerant and it is observed that thermal performances (first and second law performances) vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves (system-3) is highest and Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, individual expansion valves and flash inter coolers (system-1) is lowest.

Table 3(b): Thermodynamic performances of various vapour compression refrigeration systems using HFC-1234yf refrigerant

Performance parameters	System-1	System-2	System-3	System-4
First Law efficiency (COP_Actual)	4.972	5.188	5.227	5.017
Exergy Destruction Ratio (EDR)	2.352	2.299	2.274	2.322
Exergetic Efficiency using First Method	0.2983	0.3113	0.3136	0.301
Exergy of Fuel (kW)	42.24	40.48	40.17	41.86
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergetic Efficiency using second Method	0.2983	2845	0.2868	0.301

Table-3(b) shows the exergy destruction in various components of vapour compression refrigeration systems using R-134a refrigerant and it is observed that Vapour compression refrigeration system using multiple evaporators at different

temperatures with compound compression, multiple expansion valves and flash inter coolers (system-2) gives highest exergy destruction as compared to other systems.

Table 3(c): Exergy Destruction of various components in vapour compression refrigeration systems using HFC-1234yf refrigerant

Performance parameters	System-1	System-2	System-3	System-4
Total Exergy Destruction in compressors (%)	23.98	23.89	23.22	23.19
Total Exergy Destruction in condensers (%)	26.81	27.78	28.25	27.35
Total Exergy Destruction in evaporators (%)	9.512	12.61	12.69	9.598
Total Exergy Destruction in expansion Valves (%)	7.632	4.968	4.942	7.61
Total Exergy Destruction in sub coolers	2.166	2.244	2.23	2.149
Rational Efficiency (%)	29.83	28.45	28.68	30.1

Table-3(c) shows the exergy destruction in various components of vapour compression refrigeration systems using R-245fa refrigerant and it is observed that exergy of fuel (Electrical power required to run all compressors) of vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion

valves (system-3) is lowest and Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, individual expansion valves and flash inter coolers (system-1) is highest. It is also observed that compressor-3 gives high work done by compressor while compressor give low work done.

Table 3(d): Work done by each compressor in vapour compression refrigeration systems using HFC-1234yf refrigerant

Performance parameters	System-1	System-2	System-3	System-4
Work done by compressor -1 (kW)	2.361	1.855	8.192	10.46
Work done by compressor -2 (kW)	6.504	5.489	13.52	15.4
Work done by compressor 3 (kW)	33.37	33.13	18.46	16.01
Exergy of Fuel (kW)	42.24	40.48	40.17	41.86
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergetic Efficiency using second Method (%)	29.83	28.45	28.68	30.1

Table 4: Input conditions for evaluating thermodynamic performances of various vapour compression refrigeration systems using R-236fa refrigerant

Input Data	System-1	System-2	System-3	System-4
Refrigerant	R-236fa	R-236fa	R-236fa	R-236fa
Q_Eva1 (kW)	70	105	70	70
Q_Eva2 (kW)	105	70	105	105
Q_Eva3 (kW)	35	35	35	35
Temperature of Evaporator-1 (°C)	-5	-10	-10	-10
Temperature of Evaporator-2 (°C)	0	5	5	5
Temperature of Evaporator-3 (°C)	5	10	10	10
Temperature of condenser (°C)	40	40	40	40
Subcooling Temperature of condenser (°C)	30	30	30	30
Isentropic efficiency of compressors	0.75	0.75	0.75	0.75

Table-4(a) shows the exergy destruction in various components of vapour compression refrigeration systems using R-236fa refrigerant and it is observed that thermal performances (first and second law performances) vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves (system-3) is highest and Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, individual expansion valves and flash inter coolers (system-1) is lowest. Table-4(b) shows the exergy destruction in various components of vapour compression refrigeration systems using R-236fa refrigerant and it is observed that Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves and flash inter coolers (system-2) gives highest exergy destruction as compared to other systems. The exergy destruction in condenser is higher than compressor. For comparing all four systems, the exergy destruction in system-3 is high and lower in system-4 respectively. The exergy destruction in running all compressors of system-1 is highest while for system-4 is lowest. However the exergy destruction in all compressors is almost similar. Similarly exergy destruction in

condenser in all systems is almost similar. The exergy destruction in evaporators in System-2: Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves and flash inter coolers (system-2) is highest as compared to other systems. However exergy destruction in evaporator's system-3 has less exergy destruction than system-2 but higher than system-1 and system-4. It is also observed that exergy destruction in flash chamber is lowest. exergy destruction in expansion valves of system-4 is higher than system-1, system-2 and system3. Table-4(c) shows the exergy destruction in various components of vapour compression refrigeration systems using R-236fa refrigerant and it is observed that exergy of fuel (Electrical power required to run all compressors) of vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves (system-3) is lowest and Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, individual expansion valves and flash inter coolers (system-1) is highest. It is also observed that compressor-3 gives high work done by compressor while compressor give low work done.

Table4 (a): Thermodynamic performances of various vapour compression refrigeration systems using R-236fa refrigerant)

Performance parameters	System-1	System-2	System-3	System-4
First Law efficiency (COP_Actual)	4.973	5.226	5.264	5.182
Exergy Destruction Ratio (EDR)	2.352	2.287	2.264	2.217
Exergetic Efficiency using First Method	0.2984	0.3136	0.3158	0.3109
Exergy of Fuel (kW)	42.23	40.18	39.89	40.53
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergetic Efficiency using second Method	0.2984	0.2829	0.285	0.3109

Table 4(b): Exergy Destruction of various components in vapour compression refrigeration systems using R-236fa refrigerant

Performance parameters	System-1	System-2	System-3	System-4
Total Exergy Destruction in compressors (%)	24.4	24.3	23.8	23.65
Total Exergy Destruction in condensers (%)	26.12	27.23	27.4	27.6
Total Exergy Destruction in evaporators (%)	9.545	13.1	13.19	9.944
Total Exergy Destruction in expansion Valves (%)	8.057	4.951	4.974	6.198
Total Exergy Destruction in sub coolers	2.035	2.121	2.13	1.513
Rational Efficiency (%)	0.2984	28.29	28.5	0.3109

Table 4(c): Work done by each compressor in vapour compression refrigeration systems using HFC-236fa refrigerant

Performance parameters	System-1	System-2	System-3	System-4
Work done by compressor -1 (kW)	2.46	1.854	8.094	10.09
Work done by compressor -2 (kW)	6.648	5.476	13.28	14.9
Work done by compressor 3 (kW)	33.12	32.85	17.69	15.53
Exergy of Fuel (kW)	42.23	40.18	39.89	40.53
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergetic Efficiency using second Method (%)	29.84	28.29	28.5	0.3109

**Case-4:** In this investigation following assumptions are made by using R-245fa refrigerant:

Table 5: Input conditions for evaluating thermodynamic performances of various vapour compression refrigeration systems using R-245fa refrigerant

Input Data	System-1	System-2	System-3	System-4
Refrigerant	R-245fa	R-245fa	R-245fa	R-245fa
Q_Eva1 (kW)	70	105	70	70
Q_Eva2 (kW)	105	70	105	105
Q_Eva3 (kW)	35	35	35	35
Temperature of Evaporator-1 (°C)	-5	-10	-10	-10
Temperature of Evaporator-2 (°C)	0	5	5	5
Temperature of Evaporator-3 (°C)	5	10	10	10
Temperature of condenser (°C)	40	40	40	40
Subcooling Temperature of condenser (°C)	30	30	30	30
Isentropic efficiency of compressors	0.75	0.75	0.75	0.75

Table5 (a): Thermodynamic performances of various vapour compression refrigeration systems using R-245fa refrigerant)

Performance parameters	System-1	System-2	System-3	System-4
First Law efficiency (COP_Actual)	5.137	5.337	5.376	5.182
Exergy Destruction Ratio (EDR)	2.245	2.201	2.178	2.217
Exergetic Efficiency using First Method	0.3082	0.3202	0.3226	0.3109
Exergy of Fuel (kW)	40.88	39.35	39.06	40.53
Exergy of Product(kW)	12.6	12.6	12.6	12.6
Exergetic Efficiency using second Method	0.3082	0.2951	0.2975	0.3109

Table-5(a) shows the exergy destruction in various components of vapour compression refrigeration systems using R-245fa refrigerant and it is observed that thermal performances (first and second law performances) vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves (system-3) is highest and Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, individual expansion valves and flash inter coolers (system-1) is lowest. Table-5(b) shows the exergy destruction in various components of vapour compression refrigeration systems using R-245fa refrigerant and it is observed that Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves and flash inter coolers (system-2) gives highest exergy destruction as compared to other systems. The exergy destruction in condenser is higher than compressor. For comparing all four systems, the exergy destruction in system-3 is high and lower in system-4 respectively. The exergy destruction in running all compressors of system-1 is highest while for system-4 is lowest. However the exergy destruction in all compressors is almost similar. Similarly exergy destruction in

condenser in all systems is almost similar. The exergy destruction in evaporators in System-2: Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves and flash inter coolers (system-2) is highest as compared to other systems. However exergy destruction in evaporators system-3 has less exergy destruction than system-2 but higher than system-1 and system-4. It is also observed that exergy destruction in flash chamber is lowest. exergy destruction in expansion valves of system-4 is higher than system-1, system-2 and system-3. Table-5(c) shows the exergy destruction in various components of vapour compression refrigeration systems using R-245fa refrigerant and it is observed that exergy of fuel (Electrical power required to run all compressors) of vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, multiple expansion valves (system-3) is lowest and Vapour compression refrigeration system using multiple evaporators at different temperatures with compound compression, individual expansion valves and flash inter coolers (system-1) is highest. It is also observed that compressor-3 gives high work done by compressor while compressor 1 gives low compressor work.

